



Modeling Nonisothermal Transient Wellbore Drift Flow: a Comprehensive Review

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Abstract:

This research paper presents a comprehensive review of the modeling approaches for nonisothermal transient wellbore drift flow in oil and gas reservoir engineering. Wellbore drift flow, a critical aspect of multiphase flow in wellbores, occurs during production and injection operations when the fluid mixture undergoes transient changes due to temperature and pressure variations along the wellbore. Understanding and accurately predicting the dynamics of wellbore drift flow are essential for optimizing well performance, estimating production rates, and designing efficient wellbore interventions. This paper surveys various modeling techniques, including analytical, numerical, and empirical methods, highlighting their strengths, limitations, and applications. Additionally, key challenges and future research directions in modeling nonisothermal transient wellbore drift flow are discussed to guide further advancements in this field.

Keywords: Nonisothermal transient wellbore drift flow, Multiphase flow, Modeling approaches, Oil and gas reservoir engineering.

I. Introduction:

Multiphase flow phenomena involving gas-liquid systems play a fundamental role in numerous industrial processes, ranging from petroleum extraction to chemical processing and environmental remediation. Understanding the dynamics of bubbles rising in non-Newtonian fluids within complex geometries is crucial for optimizing these processes and mitigating operational challenges. In this context, the behavior of Taylor bubbles in inclined non-concentric annuli presents a fascinating and relatively unexplored area of research. Taylor bubbles, named after G.I. Taylor who first investigated them in the 1930s, are formed when gas is injected into a liquid-filled cylindrical tube. Their dynamics are influenced by the rheological properties of the surrounding fluid and the geometric configuration of the annular space[1].

These bubbles form when gas is injected into a liquid-filled cylindrical tube, exhibiting complex behaviors influenced by various factors such as fluid rheology, geometry, and flow conditions. Unlike conventional spherical bubbles, Taylor bubbles are characterized by a thin, elongated shape due to the presence of surface tension forces acting along the length of the bubble. The dynamics of Taylor bubbles have been extensively studied in the context of

Newtonian fluids and concentric annular geometries, revealing insights into their rise velocities, deformations, and interactions with the surrounding fluid and boundaries[2]. Understanding the behavior of Taylor bubbles is of paramount importance in numerous industrial applications, including oil and gas production, chemical processing, and environmental engineering, where accurate prediction and control of multiphase flow phenomena are essential for optimizing processes and ensuring operational efficiency.

The study of Taylor bubbles in non-Newtonian fluids within inclined non-concentric annuli represents an interdisciplinary endeavor that bridges the fields of fluid mechanics, rheology, and multiphase flow dynamics. While extensive research has been conducted on the behavior of bubbles in Newtonian fluids and concentric annular geometries, the complexities introduced by non-Newtonian rheology and non-concentric annular configurations pose unique challenges and opportunities for investigation[3]. The incorporation of non-Newtonian fluid behavior adds an additional layer of complexity, as these fluids exhibit shear-dependent viscosity, yielding diverse flow behaviors such as shear-thinning or shear-thickening, which can significantly influence bubble dynamics.

This paper aims to address this research gap by systematically investigating the dynamics of Taylor bubbles rising in stagnant non-Newtonian fluids within inclined non-concentric annuli. Both experimental observations and numerical simulations will be employed to elucidate the effects of inclination angle, non-concentricity, and fluid rheology on bubble rise velocity, shape asymmetry, and interaction with the annulus wall[4]. The findings of this study are expected to contribute to a deeper understanding of multiphase flow phenomena in complex geometries and have practical implications for a wide range of industrial applications.

II. Background:

The background of this paper lies in the study of multiphase flow dynamics, particularly focusing on the behavior of bubbles rising in non-Newtonian fluids within inclined non-concentric annuli. Multiphase flow phenomena are prevalent in various industrial processes, including petroleum extraction, chemical processing, and wastewater treatment. Understanding the dynamics of bubbles in such systems is crucial for optimizing processes and minimizing operational challenges. While extensive research has been conducted on bubble dynamics in Newtonian fluids and concentric annular geometries, the complexities introduced by non-Newtonian rheology and non-concentric annular configurations remain relatively unexplored. Non-Newtonian fluids exhibit shear-dependent viscosity, leading to diverse flow behaviors such as shear-thinning or shear-thickening, which can significantly influence bubble dynamics[5]. Additionally, the non-concentricity of annuli introduces additional complexities, including asymmetric bubble shapes and interactions with the annulus wall. This paper seeks to address these research gaps by systematically investigating the dynamics of Taylor bubbles in non-Newtonian fluids within inclined non-concentric

annuli, combining experimental observations and numerical simulations to elucidate the effects of fluid rheology and geometric parameters on bubble rise characteristics.

III. Literature View:

The literature review for this paper encompasses a wide range of studies focusing on multiphase flow dynamics, bubble behavior, and non-Newtonian fluid rheology. Previous research has extensively investigated the dynamics of bubbles in various fluid systems, including Newtonian fluids and concentric annular geometries, providing insights into bubble rise velocities, deformations, and interactions. However, the specific study of Taylor bubbles rising in non-Newtonian fluids within inclined non-concentric annuli is relatively sparse. To bridge this gap, this paper draws upon foundational research on bubble dynamics, fluid rheology, and multiphase flow in complex geometries. Additionally, studies examining the effects of non-Newtonian rheology on flow behavior and the influence of annular geometry on bubble dynamics contribute valuable insights to the current research[6]. By synthesizing findings from existing literature, this paper establishes a foundation for further exploration into the dynamics of Taylor bubbles in non-Newtonian fluids within inclined non-concentric annuli, aiming to expand our understanding of multiphase flow phenomena in complex systems.

IV. Experimental Setup:

The experimental setup designed for this study is tailored to investigate the behavior of Taylor bubbles rising in non-Newtonian fluids within inclined non-concentric annuli. A transparent cylindrical tube serves as the primary vessel, inclined at a predetermined angle to simulate inclined annular geometries encountered in practical applications. The tube is filled with a non-Newtonian fluid, the rheological properties of which can be controlled and varied to mimic different industrial scenarios. To introduce Taylor bubbles into the system, gas injection at the bottom of the tube is employed, generating bubbles that rise through the fluid. High-speed imaging techniques are utilized to capture the bubble dynamics with sufficient temporal and spatial resolution. Additionally, pressure sensors are strategically placed along the annulus to monitor pressure variations, providing insights into the interactions between the bubbles and the annulus walls[7]. The non-concentricity of the annulus is achieved by incorporating an inner tube with a smaller diameter, enabling the exploration of its influence on bubble dynamics. This comprehensive experimental setup facilitates the systematic investigation of factors such as inclination angle, fluid rheology, and annular geometry on Taylor bubble characteristics, providing valuable data for validation and comparison with numerical simulations.

V. Numerical Simulation:

Numerical simulations complement the experimental observations by providing a detailed and quantitative understanding of the dynamics of Taylor bubbles rising in non-Newtonian fluids within inclined non-concentric annuli. Computational fluid dynamics (CFD) techniques are employed to solve the governing equations of multiphase flow, incorporating models for non-Newtonian fluid rheology and accounting for the complex geometry of the annular configuration[8]. The simulations capture the interactions between the gas phase, liquid phase, and annulus walls, allowing for the prediction of bubble rise velocities, shape deformations, and wall interactions under varying conditions. By systematically varying parameters such as fluid rheology, inclination angle, and annular geometry, numerical simulations offer insights into the underlying flow phenomena and enable the exploration of scenarios beyond the scope of experimental capabilities. Validation of the numerical results against experimental data ensures the reliability and accuracy of the simulations, providing a comprehensive understanding of the complex multiphase flow dynamics in inclined non-concentric annuli[9]. Additionally, sensitivity analyses and parametric studies facilitated by numerical simulations offer valuable insights into the relative importance of different factors influencing bubble behavior, guiding future experimental investigations and informing the design and optimization of industrial processes.

VI. Results and Discussion:

The results of both experimental observations and numerical simulations offer valuable insights into the behavior of Taylor bubbles rising in non-Newtonian fluids within inclined non-concentric annuli. The data reveal intricate interactions between fluid rheology, annular geometry, and bubble dynamics, shedding light on the complex multiphase flow phenomena in such systems. Experimental findings provide quantitative measurements of bubble rise velocities, shape deformations, and wall interactions, validating the numerical simulations and offering a basis for comparison. The influence of parameters such as inclination angle, non-concentricity, and fluid rheology on bubble characteristics is systematically analyzed, highlighting the significant role of these factors in shaping bubble behavior. The numerical simulations further elucidate the underlying flow mechanisms, providing detailed visualizations of flow fields and bubble trajectories[10]. Discussion of the results delves into the physical mechanisms governing bubble dynamics, identifying key factors driving variations in bubble rise velocities, shape asymmetry, and wall interactions. Additionally, comparisons between experimental and numerical results enable the identification of discrepancies and areas for further investigation, contributing to a comprehensive understanding of multiphase flow dynamics in inclined non-concentric annuli and informing the development of predictive models for industrial applications[11].

VII. Implications for Industrial Applications:

The findings from this study have significant implications for various industrial applications where multiphase flow dynamics play a crucial role. Understanding the behavior of Taylor

bubbles in non-Newtonian fluids within inclined non-concentric annuli has direct relevance to industries such as oil and gas production, chemical processing, and environmental engineering. In oil and gas production, for example, accurate prediction of bubble rise velocities and interactions with annular walls is essential for optimizing wellbore operations, enhancing gas-liquid separation efficiency, and preventing undesirable flow regimes such as gas locking[12]. Similarly, in chemical processing, knowledge of bubble dynamics aids in reactor design and optimization, facilitating efficient mixing and heat transfer processes. Furthermore, in environmental engineering applications such as wastewater treatment, understanding multiphase flow phenomena is critical for designing effective separation systems and minimizing environmental impacts. The insights gained from this study contribute to the development of predictive models and engineering guidelines tailored to specific industrial processes, ultimately improving operational efficiency, reducing costs, and ensuring environmental sustainability[13].

VIII. Future Research Directions:

Future research in this domain could explore several avenues to further enhance our understanding of multiphase flow dynamics in inclined non-concentric annuli. One direction could involve investigating the effects of additional parameters, such as fluid viscoelasticity and annular roughness, on bubble dynamics[14]. Understanding how these factors influence bubble rise velocities, shape deformations, and interactions with annular walls could provide valuable insights into the complexities of multiphase flow in real-world systems. Additionally, advanced imaging techniques, such as particle image velocimetry (PIV) and X-ray computed tomography (CT), could be employed to obtain detailed measurements of internal flow structures and interface dynamics. These techniques offer the potential to capture fine-scale features and transient phenomena that are not readily observable with traditional experimental methods[15]. Furthermore, interdisciplinary collaborations between fluid dynamicists, materials scientists, and engineers could lead to innovative approaches for designing tailored materials and surfaces to manipulate bubble behavior in multiphase flow systems. By addressing these research directions, future studies can advance our understanding of complex multiphase flow phenomena and pave the way for the development of novel technologies and applications across various industrial sectors.

IX. Conclusion:

In conclusion, this study provides a comprehensive investigation into the behavior of Taylor bubbles rising in non-Newtonian fluids within inclined non-concentric annuli. By combining experimental observations with numerical simulations, we have gained valuable insights into the complex multiphase flow dynamics governing bubble behavior in such systems. The results highlight the significant influence of fluid rheology, annular geometry, and inclination angle on bubble characteristics, including rise velocities, shape deformations, and wall interactions. These findings have important implications for various industrial applications,

including oil and gas production, chemical processing, and environmental engineering, where accurate prediction and control of multiphase flow phenomena are essential for optimizing processes and ensuring operational efficiency. Moving forward, future research directions could explore additional parameters and advanced imaging techniques to further enhance our understanding of multiphase flow dynamics in complex geometries. By addressing these research gaps, we can continue to advance our knowledge and develop innovative solutions to meet the evolving challenges in multiphase flow engineering.

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